Dehydrogenation of 1-Phenylethanol Catalyzed by Nickel(II)diphosphine Complexes

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Abstract

Catalytic efficacy of the nickel(II)-diphosphine systems in the dehydrogenation of 1-phenylethanol to acetophenone under acceptorless conditions was investigated. Steric and electronic factors of the phosphine ligands were found to play an important role in the catalysis, while the nature of the base used and the reaction conditions, *viz.* time, tempe rature, and stoichiometry, have also shown major influence. Based on the preliminary analysis, a homogeneous path way, perhaps involving nickel hydride species, was proposed. Due to the gradual disintegration of the catalytic species, deterioration of catalytic activity was observed resulting into low to moderate conversions. Among the series of catalysts examined, the highest conversion of 52% was exhibited by the catalyst **C4**, dichloro(1,2-bis(diphenylphosphino)ethane) nickel(II) (5 mol%), when loaded with 50 mol% of sodium ethoxide in toluene at 120 °C.

Keywords: Acceptorless dehydrogenation; dehydrogenation of alcohol; nickel(II)catalyst; 1,2 bis(alkyl/arylphosphino) alkane. homogeneous catalysis; Catalyst disintegration.

1. Introduction

In recent years the acceptorless dehydrogenation process has gained much attention in academic and industrial research. It provides an efficient and atom-economical route for converting alcohols into synthetically useful carbonyl compounds, without the use of a sacrificial hydrogen acceptor. Moreover, the only byproduct formed in the reaction is highly valuable molecular hydrogen.[1–3] Due to the vast significance of this catalytic reaction, a variety of homogeneous catalysts has been developed and employed in this process. It is often seen that the catalysts containing precious metal centres, viz., Ru, Rh, Ir, and Os have exhibited better performance,[4–7] nevertheless, with the meticulous tuning of structural features of the catalyst and reaction conditions, systems containing sustainable metals such as Fe, Co and Mn were also shown to exhibit comparable activities in this catalytic reaction.[8–15] However, in comparison, nickel-based catalysts are underexplored in dehydrogenation chemistry; examples of single-molecule nickel catalysts capable of mediating acceptorless dehydrogenation of alcohols are extremely scarce. Key examples are the Ni(II) complexes supported by tris(3,5-dimethylpyrazolyl)borate and 2-hydroxyquinoline mixed ligands developed by Jones *et al.*[16] and Ni(II) complexes derived from 2,6-bis(diethylaminomethyl)pyridine) pincer ligand reported by Zhang *et al.*[17] It is important to notice that these catalysts involve either exotic ligand systems or special reaction conditions to achieve the desired reactivity. This prompted us to look for simple nickel-based systems, which can efficiently catalyse dehydrogenation of alcohols under mild to moderate reaction conditions. Incidentally, diphosphine nickel(II)chloride complexes attracted us due to their simple synthetic protocols, stability and well-established catalytic profile.[18–25] Here in this article, we describe the use of diphosphine nickel(II)chloride complexes in the acceptorless dehydrogenation of alcohols.

2. Experimental

All of the synthesis and catalysis procedures were performed under N_2 atmosphere using Schlenk line techniques. All the solvents and reagents used in this work were

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purified & dried using standard protocols[26] and stored over molecular sieves (4 Å). Ligands, bis(dimethylphosphaneyl)ethane (**L1**), bis(diethylphosphaneyl)ethane (**L2**), bis(diphenylphosphaneyl)ethane (**L4**), triphenylphosphine (**L5**), bis(diphenylphosphaneyl)methane (**L6**), 1,3-bis(diphenylphosphaneyl)propane (**L7**) were purchased from Sigma Aldrich (Merck). Ligand, bis(diisopropylphosphaneyl)ethane (**L3**)[27] and the nickel(II)catalysts, [1,2-bis(dimethylphosphino)ethane]dichloronickel(II) (**C1**),[28] [1,2-bis(diethylphosphino)ethane]dichloronickel(II) (**C2**),[28,29] [1,2 bis(diisopropylphosphino)-ethane]dichloronickel(II) (**C3**),[30] [1,2-bis(diphenylphosphino)ethane]dichloronickel(II) (**C4**),[28,31] dichlorobis(triphenylphosphine)nickel(II) (**C5**),[32] bis(diphenylphosphino)methane] dichloronickel(II) (**C6**)[31] and bis(diphenylphosphino)propane]dichloronickel(II) (**C7**)[31], were prepared by following the reported protocols.
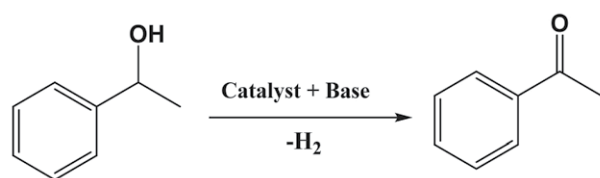
Scheme 1: Catalytic acceptorless dehydrogenation of 1-phenyl ethanol

In a typical catalytic acceptorless dehydrogenation reaction (Scheme 1), 0.05 mmol of nickel(II)phosphine catalyst (**C1–C7**) and 0.5 mmol of base were loaded in a two necked Schlenk flask equipped with a water condenser under N_2 atmosphere. 2 mL of toluene (dried over benzophenone-sodium) was added and the mixture was stirred for a couple of minutes. 0.122 mL (1 mmol) of 1-phenylethanol was added to the catalytic mixture using a syringe and the Schlenk flask was kept in a 120 °C preheated oil-bath and stirred vigorously for 16 h. A continuous bubbling of N_2 gas was maintained throughout the reaction. After the scheduled period of time, the reaction was stopped, allowed to cool to room temperature and opened to air. The product yield was analysed by gas chromatography analysis (*vide infra*) and in some cases, also by ^{1}H NMR spectroscopic analysis (*vide infra*). Product isolation was done by running the catalytic mixture through a silica gel column using ethyl acetate:hexane (1:3) eluant. The results are summarized in Table 1.

GC analysis details: After the reaction, the reaction mixture was diluted with 9 mL of dichloromethane and filtered through a short plug of Celite. 360 μL of filtrate and 25 μL of tridecane (internal standard) were taken in 3mL of dichloromethane and analyzed on Shimadzu GC-17A – FID instrument, using Agilent DB-WAXETR column (30 m × 0.25 mm, thickness 0.50 μm) using helium as a carrier gas. Method used: starting oven temperature, 50 °C (hold for 5 min); maximum temperature, 240 °C; heating rate, 15 °C/min (hold for 5 min); column pressure: 24.5 psi; total flow: 273 mL/min, column flow: 2.64 mL/min, split ratio: 100, linear velocity: 49 cm/sec.

^{1}H NMR spectroscopic analysis details: Reaction mixture was evacuated under a weak vacuum to partially remove the solvent (toluene), followed by the addition of ~ 0.3 mL of $CDCl_3$ and thorough mixing. An aliquot from this solution was taken in an NMR tube, diluted with $CDCl_3$ and analyzed on a Bruker Ascend 500 NMR spectrometer operating at 500 MHz at RT). Relative area of integration of the methyl protons of 1-phenylethanol
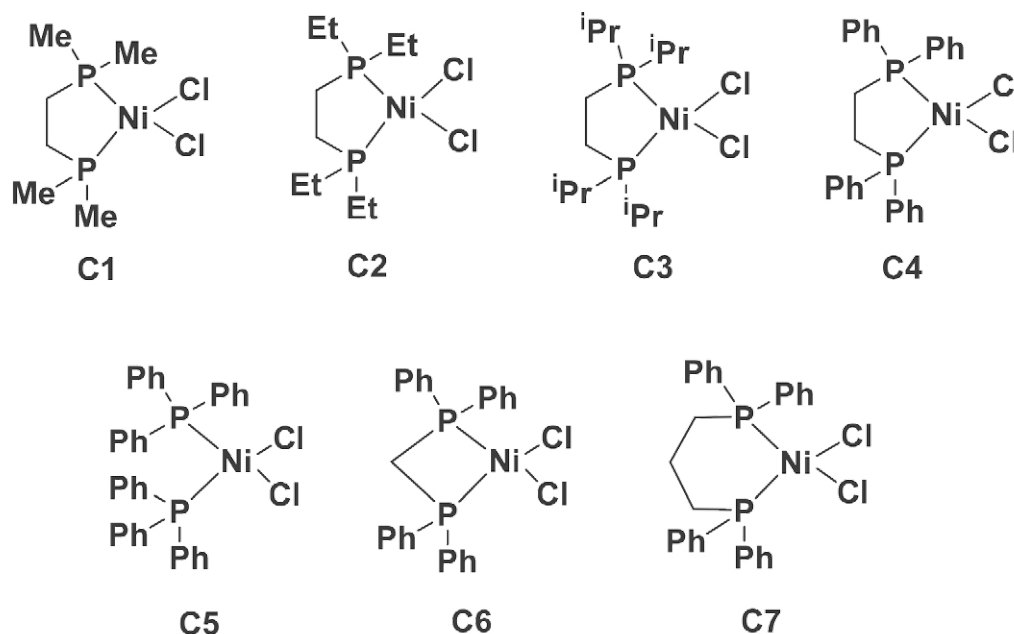

Figure 1: Nickel(II)diphosphine complexes used in the current study.

(doublet or broad, ~ δ 1.48) and acetophenone (singlet, ~ δ 2.57) were considered to calculate the percent of conversion.

^{31}P{^{1}H} NMR analysis was done in CDCl$_3$ on a Bruker AMX 400 spectrometer operating at 162 MHz at RT; Chemical shift values are reported with reference to the external standard, H$_3$PO$_4$. In the analysis of catalytic mixture, an aliquot of reaction mixture was taken in NMR tube, added with CDCl$_3$ and used for analyses.

3. Results and Discussion

Among the nickel(II)complexes supported by the substituted diphosphinoethane ligands (Figure 1), we found that the system bearing phenyl substitutions (i.e., **C4**) exhibited better activity, converting 52% of 1-phenylethanol to acetophenone, under the current reaction conditions (Entry 4, Table 1). The systems having methyl (**C1**) and isopropyl (**C3**) substitutions on the phosphorus donors yielded only 12 and 14% of acetophenone, respectively (Entries 1 and 3 in Table 1). With the nickel(II)diphosphine system substituted with ethyl groups on phosphorus, 30% conversion was observed (Entry 2, Table 1). This indicates the significant influence of electronic effects of the ligands on the stability and reactivity of the catalyst system.[33,34] Incidentally, anhydrous nickel(II)chloride in the absence of any phosphine ligand showed no detectable conversions under our reaction conditions (Entry 8, Table 1). Sole use of the ligand, bis(diphenylphosphaneyl)ethane

(L4) did not provide any catalytic conversion (Entry 9, Table 1). Sodium ethoxide (50 mol%) in absence of nickel catalyst also did not show any detectable conversion (Entry 10, Table 1).

Table 1: Catalysis data for acceptorless dehydrogenation of 1-phenylethanol to yield acetophenone; catalyzed by nickel(II)diphosphine complexes **C1–C7**.*

Entry	Catalyst	Conversion (%)[#]	Yield (%)[$]
1	**C1**	12	–
2	**C2**	30	24
3	**C3**	14	–
4	**C4**	52	45
5	**C5**	30	25
6	**C6**	21	16
7	**C7**	34	26
8	NiCl$_2$	NIL	–
9	**L4**	NIL	–
10	–	NIL	–

*Catalytic reactions are conducted in dry toluene with 1mmol of 1-phenyl ethanol, 0.05 mmol of catalyst (5 mol%) and 0.5 mmol (0.027 g, 50 mol%) of NaOEt, at 120 °C (oil bath temperature) for 16h, under the slow, continuous bubbling of nitrogen gas. [#] Data from GC analysis (Average value of two duplicate experiments). [$] Isolated yield.

Further, we examined the efficacy of different phosphinonickel(II)chloride complexes, bearing phenyl substituents on the phosphorus but with varying spacer groups in the acceptorless dehydrogenation of 1-pheny-

Table 2: Catalysis data for acceptorless dehydrogenation of 1-phenylethanol to yield acetophenone; catalyzed by the nickel(II)diphosphine complex **C4** under various reaction conditions.

Entry	Catalyst (mol%)	Base (mol%)	Reaction conditions	Conversion (%)*	Yield (%)[#]
1	**C4** (5)	NaOEt (50)	120 °C in Toluene, 16h, No N$_2$ bubbling.	8	–
2	**C4** (5)	NaOMe (50)	120 °C in Toluene, 16h, With N$_2$ bubbling.	23	15
3	**C4** (5)	KOH (50)	120 °C in Toluene, 16h, With N$_2$ bubbling.	4	-
4	**C4** (5)	KO^{t}Bu (50)	120 °C in Toluene, 16h, With N$_2$ bubbling.	50	45
5	**C4** (5)	NaOEt (25)	120 °C in Toluene, 16h, With N$_2$ bubbling.	22	16
6	**C4** (5)	NaOEt (10)	120 °C in Toluene, 16h, With N$_2$ bubbling.	11	–
7	**C4** (10)	NaOEt (50)	120 °C in Toluene, 16h, With N$_2$ bubbling.	56	48
8	**C4** (2)	NaOEt (50)	120 °C in Toluene, 16h, With N$_2$ bubbling.	12	–
9	**C4** (5)	NaOEt (50)	120 °C in Toluene, 24h, With N$_2$ bubbling.	54	45
10	**C4** (5)	NaOEt (50)	120 °C in Toluene, 48h, With N$_2$ bubbling.	55	45
11	**C4** (5)	NaOEt (50)	120 °C in Toluene, 8h, With N$_2$ bubbling.	32	24
12	**C4** (5)	NaOEt (50)	25 °C in Toluene, 16h, With N$_2$ bubbling.	Traces	–
13	**C4** (5)	NaOEt (50)	60 °C in Toluene, 16h, With N$_2$ bubbling.	8	–
14	**C4** (5)	NaOEt (50)	140 °C in Xylenes, 16h, With N$_2$ bubbling.	54	45
15[Ψ]	**C4** (5)	NaOEt (50)	120 °C in Toluene, 16h, With N$_2$ bubbling.	46	38
16[¥]	**C4** (5)	NaOEt (50)	120 °C in Toluene, 16h, With N$_2$ bubbling.	54	44
17[##]	**C4** (5)	NaOEt (50)	120 °C in Toluene, 16h, With N$_2$ bubbling	52	43
18[$]	**C4** (5)	NaOEt (50)	120 °C in Toluene, 16h, With N$_2$ bubbling.	51	43

*Data from GC analysis (Average value of two duplicate experiments; Percent of conversion obtained from ^{1}H NMR spectroscopic analysis were comparable with the GC data, within the difference of ± 5%). [#] Isolated yield. [Ψ]1-(p-tolyl)ethanol was used as substrate. [¥] 1-(4-fluorophenyl)ethanol was used as substrate. [##]A drop of metallic mercury (~ 50 mg) was added to the reaction mixture prior heating (Mercury poisoning test). [$]A drop of carbon disulphide (~ 0.1 mL) was added to the reaction mixture prior heating (CS$_2$ poisoning test).

lethanol, under the same reaction conditions. It was found that the phenylphosphine(II)nickel system with a propyl (three-carbons) spacer (**C7**) exhibited better activity yielding 34% of acetophenone (Entry 7, Table 1), over the system bearing a methylene (one-carbon) spacer (**C6**), which could dehydrogenate only 21% of the substrate (Entry 6, Table 1). On the other hand, the catalytic activity of the nickel catalyst containing two triphenylphosphine ligands (**C5**) was found to fall between the complexes **C6** and **C7** (30% conversion, Entry 5, Table 1). Nevertheless, the complex, **C4**, which bears an ethyl (two carbon) spacer was found to be the best catalyst among the systems employed in this study (Entry 4, Table 1), hence was chosen for the further exploration. The higher activity of the complex **C4** can be correlated with its higher stability. Due to the presence of a stable five membered coordination ring (ring size effect) and near ideal bite angle β, this system is expected to be stabilized electronically.[34–38]

Continuous bubbling of dry nitrogen/argon gas throughout the reaction period is found to be key to expel the molecular hydrogen produced and to access the better conversions.[16] A drastic decrease in the yield (~8%) was observed, otherwise, due to the superseding backward, hydrogenation reaction[31] (Entry 1, Table 2). Since alcohol dehydrogenation is a thermodynamically uphill process,[39] continuous removal of hydrogen gas will have a positive thermodynamic contribution and can favour the forward reaction.[40]

The nature and stoichiometric ratio of the base used play an important role in the dehydrogenation-hydrogenation catalytic reactions.[41] In the current studies, sodium ethoxide was found to be the most compatible base; replacing it with sodium methoxide, under similar reaction conditions, yielded lower conversion *viz.*, 23% (Entry 2, Table 2). Potassium hydroxide was found to be unsuitable for our system, which produced only about 4% of acetophenone (Entry 3, Table 2), while potassium tert-butoxide provided a comparable yield (50 % conversion, Entry 4, Table 2). Lowering the loading of the base sodium ethoxide to 25 mol% (Entry 5, Table 2) or 10 mol% (Entry 6, Table 2) resulted in a decrease in reactivity, yielding 22% and 11% of the product, respectively, indicating that the higher loading of 50 mol% of base is essential to maintain the catalytically active species during the course of the reaction.[41,42]

In an attempt to improve the catalytic conversion, we tried varying the catalyst loading, keeping the stoichiometry of the sodium ethoxide unchanged (50 mol%) under the same reaction conditions. When the catalyst loading was increased to 10 mol% (Entry 7, Table 2) a slight improvement in the conversion (56%) was observed, indicating that higher catalyst loading is necessary to get better conversions. Conversely, when catalyst loading was reduced to 2 mol% (Entry 8, Table 2), a drastic decrease in the activity was observed, yielding only 12% conversion.

All the catalytic reactions in the above studies were run overnight (16h). In anticipation of increasing the con-

version, we extended the reaction period to 24h (Entry 9, Table 2). This resulted in a slight enhancement in the conversion providing 54% of the product. However, further extension of the reaction period to 48h did not show any significant improvement in the yield (Entry 10, Table 2), indicating gradual degeneration of the catalytic species over time.[42] On the other hand, when the reaction time was limited to 8h, only 32% conversion was observed (Entry 11, Table 2).

To overcome the thermodynamic constraints, the process of dehydrogenation of alcohols often requires higher reaction temperatures[16] or a suitable acceptor.[43] In our current acceptorless reaction conditions, we found that a higher reaction temperature, *viz.* 120 °C, is required to attain higher conversions. When the catalytic reaction was carried at room temperature (Entry 12, Table 2), no detectable catalytic activity was observed and the reaction conducted at 60 °C (Entry 13, Table 2) yielded only 8% conversion. On the other hand, when the reaction was conducted at higher temperature (140 °C, in xylenes), a slight improvement in the activity was observed, providing 54% conversion (Entry 14, Table 2).

Further, we examined the efficacy of our catalytic system in the dehydrogenation of a couple of *para* substituted 1-phenylethanol motifs. The substrate containing an electron donating group, 1-(*p*-tolyl)ethanol (Entry 15, Table 2), yielded slightly lower conversion (slower reaction) compared to the substrate bearing an electron withdrawing substituent, 1-(4-fluorophenyl)ethanol (Entry 16, Table 2) under the same reaction conditions. This reactivity pattern is in line with the earlier observations involving nickel-based catalysts.[16] Due to the moderate reactivity of the catalyst system, we did not try to expand the substrate scope to other alcholols.

It has recently been shown that nickel(II)diphosphine complexes are very good catalysts in transfer hydrogenation, where various substituted ketones were converted nearly quantitatively to the corresponding alcohols using isopropanol as a sacrificial hydrogen donor as well as a solvent.[31] However, in the current acceptorless conditions, in spite of our attempts with varying reaction stoichiometry and conditions, we were not able to improve the conversion. Gradual disintegration of the catalyst under the reaction conditions is envisaged to be the main cause for the deterioration of catalytic activity. However, the dominant backward hydrogenation reaction could also have some key role to play.[16,31] During the course of the catalytic dehydrogenation reaction, a change in the colour of the reaction mixture from yellow to dark brown was observed, which is a typical indication for the formation of Ni(0) related nanoclusters.[31,44] In order to investigate if the Ni(0) nanoclusters have any role to play in the catalysis, a mercury poisoning test (Entry 15, Table 2),[16,47] as well as a carbon disulphide poisoning test (Entry 16, Table 2)[46] were performed. However, both tests turned out to be negative, as no significant difference in the catalytic reactivity/

conversion was observed, thus, ruling out any contribution from a metal nano-particle mediated heterogeneous pathway.[41] Further, in the $^{31}P\{^1H\}$ NMR spectroscopic analysis, we found that, a single signal at δ 57.1 observed for the complex C4, experiences a significant shift upon addition of 2 equivalent amount of 1-phenyl ethanol and heating to 60 °C for five minutes with thorough shaking, forming a peak at δ 33.0 indicating the formation of a new compound, possibly an alkoxide species. Same signal (~ δ 33.0) was observed in the $^{31}P\{^1H\}$ NMR spectrum of the catalytic mixture, when recorded at the initial stages (within 5 min), suggesting the formation of the same species as in the catalytic conditions. However, at the end of the catalytic reaction (24h), the appearance of a new signal at δ 198.5 along with the signal at ~ δ 33.0 indicates partial dissociation of the intermediate compound. All of these observations strongly suggest a catalytic mechanism involving a homogeneous route, perhaps mediated by nickel alkoxide and nickel hydride intermediates, as envisaged in the previous studies.[16,31,47]

4. Conclusion

Overall, we have explored the catalytic efficacy of the nickel(II)diphosphine systems in the dehydrogenation of 1-phenylethanol under acceptorless conditions. Steric and electronic factors of the phosphine ligands were found to play an important role in the catalysis along with the nature of the base used, as well as the reaction conditions. The catalytic reaction was found to follow a homogeneous pathway, presumably involving nickel hydride species. The catalytic reaction suffers mostly due to the disintegration of the catalytic species, providing only low to moderate conversions. We are currently working on isolation of the nickel hydride species, as structural characterization of these reactive intermediates could help us in understanding the mechanistic aspects of the catalytic reaction which would, indeed, help in improving the efficacy and expanding the substrate scope of the catalytic systems.[48,49] Perhaps, these systems can be tuned to efficiently promote Guerbet upgrading of ethanol to n-butanol, which is a reaction of great commercial importance and of our primary focus.[41,50]

5. References

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Povzetek

Proučili smo katalitično učinkovitost sistema nikelj(II)-difosfin pri dehidrogenaciji 1-feniletanola do acetofenona brez prisotnosti akceptorja. Ugotovili smo, da imajo sterični in elektronski faktorji fosfinskega liganda pomemben vpliv na katalitične lastnosti sistema, pomembna pa je tudi izbira baze ter reakcijskih pogojev (čas reakcije, temperatura, stehiometrija). Glede na preliminarne analize predvidevamo homogen mehanizem, morda z udeležbo zvrsti, ki vsebuje nikljev hidrid. Nizke konverzije so posledica zmanjšanja katalitične aktivnosti sistema zaradi počasnega razkroja katalitične zvrsti. Med proučevanimi katalizatorji ima največjo konverzijo (52 %) katalizator **C4**, dikloro(1,2-bis(difenilfosfino) etan)nikel(II) (5 mol%), ob dodatku 50 mol% natrijevega etoksida v toluenu pri 120 °C.